## SPECIFICATION AMENDMENTS

On page 1, insert above line 1, insert--Priority Claim

The present application claims priority on European Patent Application 04251319.2 filed 8 March 2004.--

On page 1, above line 1, insert--Field of the Invention--

On page 1, above line 9, insert--Background of the Invention--

The paragraph on line 29 of page 2, and ending on line 20 of page 3 has been amended as follows:

--The use of liquid recycles as a means of improving the overall performance in a fixed-bed design has been described. Such a system is also called a "trickle bed" reactor (as part of a sub set of fixed-bed reactor systems) in which both reactant gas and liquid are introduced (preferably in an up flow or down flow orientation with respect to the catalyst) simultaneously. The presence of the flowing reactant gas and liquid improves the reactor performance with respect to CO conversion and product selectivity. A limitation of the trickle bed system (as well as of any fixed-bed design) is the pressure drop associated with operating at high mass velocities. The gas-filled voidage in fixed-beds (typically less than 0.50) and size and shape of the catalyst particles does not permit high mass velocities without excessive pressure drops. Consequently, the mass through-put undergoing conversion per unit reactor volume is limited due to the ~~head~~ heat transfer rates. Increasing the individual catalyst particle size may slightly improve the heat transfer by allowing higher mass velocities (for a given pressure drop), but the loss in selectivity towards the high boiling point products and the increase in methane selectively combined with the increase in catalyst activity generally offset the commercial incentives of higher heat transfer.--

The paragraph on line 15 of page 5has been amended as follows:

-- US patent 6,344,490 describes a three phase slurry bubble column comprising one or more filter assemblies suspended in a slurry. The construction of the reactor and the filter assemblies is such that each assembly can be removed via an

opening in the top of the reactor. From the description it is clear that the change ~~chance~~ is done at ambient pressure. Thus, in the case that one or more filters need to be replaced in the process according to US 6,344,490, the process needs to be stopped, the reactor needs to be depressurised, and a restart (at high pressure and high temperature) needs to be done. For a large commercial slurry reactor it will take several hours to cool down the reactor by 75-100 °C, depressurisation, filter exchange, repressurisation and heating up by 75-100 °C.--

On page 5, above line 30, insert--Summary of the Invention--

On page 6, after line 2, insert--Brief Description of the Drawings

Without wishing to be restricted to a particular embodiment, the invention will now be described in further detail with reference to the drawings in which:

Figure 1 is a side view of a general arrangement of a reactor having a filter system;

Figure 2 is plan view of the reactor of Fig. 1, showing the arrangement of filters around the pipework of the Fig. 1 reactor;

Figure 3 is a side view of a filter system of the Fig. 1 reactor;

Figure 4 is a side view showing the detail of the filter module; and

Figure 5 is a cross-sectional view of a filter module.--

On page 6, above line 3, insert--Detailed Description of the Invention--

The paragraph on line 3 of page 6 has been amended as follows:

-- An ~~The~~ advantage of the present invention is that it is not ~~needed any more~~ necessary to stop the process, cool down the inventory and to re-pressurize ~~pressurise~~ and heat up the reactor to ~~till~~ the reaction temperature in order to remove the filter. Suitably the reaction temperature is decreased by 25-75 °C, i.e. just sufficient to stop the reaction. The amount of synthesis gas introduced in the reactor may be decreased by up to 75%. At least 10%, preferably about 20% is usually still introduced in the reactor in order to keep the catalyst particles in suspension. The remaining syn gas stream may be replaced by another gas, e.g. an inert gas as nitrogen or by a recycle stream. Preferably the reaction the reactor temperature is decreased by

less than 25 °C, preferably less than 10 °C, and the reaction is continued at the same productivity as the continuous productivity.--

On page 10, delete line 9-21.

On page 21, above line 1, insert--We claim:--